SIMULATION OF THE FLUID-STRUCTURE INTERACTION INVOLVING TWO-PHASE FLOW AND HEXAGONAL STRUCTURES IN A NUCLEAR REACTOR CORE

S. HOUBAR 1 , A. GERSCHENFELD 1 AND G. ALLAIRE 2

 1 DES - Département de Modélisation des Systèmes et Structures (DM2S) CEA, Université Paris-Saclay, F-91191 Gif-sur-Yvette, France sofiane.houbar@cea.fr, antoine.gerschenfeld@cea.fr

² Centre de Mathématiques Appliquées, École Polytechnique, Institut Polytechnique de Paris route de Saclay, 91128 Palaiseau Cedex, France gregoire.allaire@polytechnique.fr

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Abstract. In order to enhance safety assessments of Sodium Fast Reactors (SFR), some scenarios involving transient Fluid-Structure Interactions (FSI) are investigated using numerical simulation tools. SFRs are indeed quite sensible to mechanical deformations regarding their nuclear power (see [1] for more details). The originality of the scenario presented in the paper is to consider sufficient large mechanical interactions involving a large pressure decrease in the fluid domain. This decrease leads to vaporization of the fluid and then to a different impact on the structures. By means of the open-source software *Code Saturne* developed by EDF [2], this scenario is investigated in 2D using a 3-equation model derived from the Navier-Stokes equations while an harmonic model is applied for the mechanical structures. The code coupling is managed using the Newmark algorithm for the mechanical part and a damped fixed point algorithm in order to get a converged coupled FSI problem.

1 INTRODUCTION

In the framework of the Generation IV International Forum [3] gathering countries involved in the development of the future nuclear reactors, various scenarios are investigated using the numerical simulation tool in order to demonstrate their reliability. Some of those scenarios include complex phenomena by coupling different physics. One of this kind of scenarios concern the impact of mechanical deformations of the core which may have an impact on the safety of the reactor core.

In order to perform the numerical simulation of such phenomena, a correct code coupling framework has to be established in order to avoid numerical instabilities and numerical diffusion / dissipation.

Hence, this paper aims at specifying the algorithms used within the Finite Volume code *Code Saturne* (v6.0.1) in order to simulate the fluid-structure interaction involving inter-wrapper flows and hexagonal structures. This case corresponds to a strong coupling due to the thin hydraulic inter-wrapper domain.

Figure 1: 3D view of a SFR core Figure 2: Cross-sectional view of the Phénix reactor core

2 PRESENTATION OF THE CONTEXT OF THE STUDY

2.1 SFR core design

SFR cores are made of slender hexagonal structures which are highly packed. They are composed with fuel sub-assemblies exchanging the extracted thermal power with circulating liquid sodium (see the mock-up depicted in Figure 1).

Within the French design, these fuel assemblies are fixed at the bottom and can potentially move. The space between them is filled with stagnant liquid sodium as long as the structures are not moving. The sketch in Figure 2 represents then a geometrical modelling of such a core.

If such cores are subjected to mechanical excitations (see [4]), complex FSI phenomenon may appear due to liquid sodium recirculation in the inter-wrapper region.

2.2 Methodology: a reference case

In case of mechanical excitation, the assemblies may move inwards or outwards involving a flow recirculation as depicted in Figure 3. Consequently, the flow recirculation induces a pressure field in the hydraulic region.

3 HYDRAULIC PHENOMENOLOGY

3.1 Presentation of the local scale

In order to find an law for this field, we consider the simplified case composed with top-bottom plates as depicted in Figure 4.

Figure 3: First ring of assemblies in steady state (left) and excited state (right)

Figure 4: Fluid in steady state (left) and movement induced by moving boundaries (right)

3.2 Mathematical framework

In order to model the fluid part, we use the classical Navier-Stokes equations. In order to take into account the movement of the top/bottom boundaries, the ALE (*Arbitrary Lagrangian-Euler*) technique is used (see for example [5] for the mathematical details of the method). As a consequence, the grid velocity u_w is included in Equation (1).

With respect to Figure 4, the following notations are used in order to identify the domain where the Navier-Stokes are solved and where the boundary conditions are set:

$$
\Omega(t) \stackrel{def}{=} [-L/2, L/2] \times [-h(t)/2, h(t)/2]
$$

\n
$$
\partial \Omega_1(t) \stackrel{def}{=} \left\{ (x, y) \in \mathbb{R}^2, |x| = \frac{L}{2} \right\}, t \in \mathbb{R}^+
$$

\n
$$
\partial \Omega_2(t) \stackrel{def}{=} \left\{ (x, y) \in \mathbb{R}^2, |y| = \frac{h(t)}{2} \right\}, t \in \mathbb{R}^+
$$

\n
$$
\partial \Omega_2^-(t) = \partial \Omega_2(t) \cap \{y < 0\}
$$

\n
$$
\partial \Omega_2^+(t) = \partial \Omega_2(t) \cap \{y > 0\}
$$

According to these notations, the local hydraulic problem is set as follows:

$$
\nabla \mathbf{u} = 0 \text{ in } \Omega(t)
$$
\n
$$
\partial_t \mathbf{u} + [(\mathbf{u} - \mathbf{u}_{\mathbf{w}}) \cdot \nabla] \mathbf{u} = -\frac{1}{\rho} \nabla P + \nu \Delta \mathbf{u} \text{ in } \Omega(t)
$$
\n
$$
P|_{\partial \Omega_1} = P_{\infty}
$$
\n
$$
\mathbf{u}|_{\partial \Omega_2^-} = \xi^-
$$
\n
$$
\mathbf{u}|_{\partial \Omega_2^+} = \xi^+
$$
\n(1)

Depending on the movement of the top/bottom boundaries, $\Omega(t)$ changes its volume. It induces a mass conservation depending on time in the volume $V_x(t)$ which is graphically represented in Figure 5.

Figure 5: Illustration of the mass conservation law within a hydraulic channel

3.3 Establishing a mutual influence between hydraulics and mechanics

Regarding the previous subsection, a movement of the boundaries, corresponding to the displacement of the structures, involves a change in the pressure field. An analytical pressure field can be then found assuming a velocity pattern which respects the mass conservation property in $\mathcal{V}_x(t)$:

$$
\int_{\partial \mathcal{V}_x(t)} \mathbf{u} \cdot \mathbf{d}S = 0 \tag{2}
$$

Then, we get an equality for the averaged streamwise velocity (with $u_x \stackrel{def}{=} \mathbf{u_x} \cdot \mathbf{e_x}$):

$$
\langle u_x \rangle \stackrel{\text{def}}{=} \frac{1}{h(t)} \int_{h(t)} u_x \, dy = -\frac{h'(t)}{h(t)} x \tag{3}
$$

This relationship allows us to find an expression for the averaged pressure over the spanwise direction *y* designated as $\langle P(x, y, t) \rangle$. The details of the resolution can be found in [6].

$$
\langle P(x, y, t) \rangle = P_{\infty} + \frac{\rho}{2h} \left[\left(h'' - \frac{h'^2}{h} \right) - A_n \frac{h'^2}{h} \right] \left[x^2 - \left(\frac{L}{2} \right)^2 \right] + \frac{\alpha \rho v^{\beta}}{2^{2 + \beta} (3 - \beta)} \left[h^{-3} |h'|^{1 - \beta} h' \right] \left[|x|^{(3 - \beta)} - \left(\frac{L}{2} \right)^{3 - \beta} \right]
$$
\n(4)

with $A_n \in \mathbb{R}^+$ a factor close to 1 depending on the velocity profile and (α, β) a couple of parameters chosen for the friction law represented in the Equation 5:

$$
\int_{h(t)} \mathsf{v} \Delta u_x dy = -\frac{1}{2D_h} f \vert < u_x > \vert < u_x > \, f = \alpha (Re_x)^{\beta} \tag{5}
$$

with D_h depicting the hydraulic diameter and Re_x the Reynolds number based on the mean velocity $\langle u_x \rangle$.

This analytical expression applied at the local scale (Figure 4) has shown good agreements with numerical simulation results from different CFD codes (see [6]).

In addition, it can be shown that the pressure law in Eq. 4 can be easily extended to the radial channel such as I_0 or I_2 (see Figure 13) by adapting changes in the boundary conditions.

3.4 Pressure evolution with mechanical forcing

Using Equation (6), pressure evolution at a local scale depending on the *a priori* known excitation $h(t)$ can be investigated. We choose to consider an excitation corresponding to a free harmonic system in order to evaluate its effects on the pressure field in the fluid part.

$$
h(t) = h_n (1 + a \cos(\omega t))
$$
\n⁽⁶⁾

with *h_n* the nominal spacing between the structures, $a \stackrel{def}{=} \frac{h_{max} - h_{min}}{h_{max} - h_{min}}$ $h_{max} + h_{min}$ the expansion factor and ω the pulsation of the movement. It can be seen in Figure 6 and Figure 7 that, for a fixed frequency value, the convective term plays a different role depending on the factor *a*. As a result, the effect of the fluid forces on the structures is different whether the amplitude of the displacement is relatively small or not.

Figure 6: Pressure evolution with $a = 0.05$

Figure 7: Pressure evolution with $a = 0.5$

Figure 8: Isovalues of the minimum pressure in the domain (f, a_{min})

By including Eq. (6) in (4) , we get that the minimum pressure is only due to the second derivative h'' . Figure 8 show the graphical illustration of the conditions on the minimum spacing *hmin* or frequency of the displacement *f* in order to reach a minimum pressure.

Moreover, the length of the channel *L* plays a role in the quantification of the pressure decrease.

3.5 Pressure evolution and Cavitation

When the value of $\langle P \rangle$ corresponds to the saturation pressure P_{sat} , a specific modelling has to be used in order to take into account the co-existing vapour and liquid phases. A mixture 3-equation model is used. In our case, we use the Merkle's model (see [7]):

$$
\frac{\nabla \cdot \mathbf{u}_{\mathbf{m}}}{\text{mass balance}} = \frac{\Gamma_{\nu}}{\text{exchange term}} \left(\frac{1}{\rho_{\nu}} - \frac{1}{\rho_{l}} \right) \tag{7}
$$
\n
$$
\frac{\partial_{t} \rho_{m} \mathbf{u}_{\mathbf{m}}}{\text{unsteadians}} + \underbrace{(\mathbf{u}_{\mathbf{m}} - \mathbf{u}_{\mathbf{w}}) \cdot \nabla (\rho_{m} \mathbf{u}_{\mathbf{m}})}_{\text{convection}} = \frac{-\nabla P}{\text{driving source}} + \underbrace{\mu \Delta \mathbf{u}_{\mathbf{m}}}_{\text{friction}}
$$
\n
$$
\frac{\partial_{t} \alpha}{\partial t} + \underbrace{[-\mathbf{u}_{\mathbf{w}} \cdot \nabla (\mathbf{u}) + \nabla \cdot (\alpha \mathbf{u})]}_{\text{transport}} = \frac{\Gamma_{\nu}}{\rho_{\nu}}
$$
\n(7)

with u_m the mixture velocity, ρ_m the mixture density, α the void fraction and $\Gamma_v = m^+ + m^-$ such as:

$$
\dot{m}^+ = -\frac{\rho_l \min\left(P - P_{sat}, 0\right) \alpha (1 - \alpha)}{t_{\infty} P_{sat}} \tag{8}
$$

$$
\dot{m}^- = -\frac{\rho_v \max\left(P - P_{sat}, 0\right) \alpha (1 - \alpha)}{t_{\infty} P_{sat}} \tag{9}
$$

with $t_{\infty} = 1$ ms.

Let us consider the channel case depicted in Figure 4. The application within a refined mesh of such a model compared to the case without cavitation is shown in Figures 9 and 10. The pressure remains constant at $P = P_{\text{sat}}$ where the void fraction field is not negligible.

Figure 9: Pressure evolution over (Ox)

Figure 10: Pressure versus time at the center of the hydraulic channel

3.6 Multi-1D modelling

Despite complex phenomena occurring in the hydraulic part in case of mechanical excitation, it would be too costly regarding time and computing resources to consider a refined mesh over the whole hydraulic domain such as depicted in Figure 11. As a consequence, a multi-1D model has been considered in order to reduce the cost of the calculations (Figure 12). Within this modelling, only mass conservation, regular and singular pressure drop are considered.

The details of the equations using the multi-1D modelling can be seen in [1].

4 FLUID-STRUCTURE INTERACTION

4.1 FSI modelling

The general formulation for a damped mass-spring system is considered in order to model the mechanical part as follows (here in tensor notation):

$$
\underline{M_i} \underline{\ddot{X}_i} + \underline{C_i} \underline{\dot{X}_i} + \underline{K_i} \underline{X_i} = \sum_j \underline{F_{Fl \to St}} \big|_{\partial I_j} \tag{10}
$$

with the I_j the hydraulic channels in connection with the assembly A_i such as depicted in the 3D sketch of Figure 13.

The mechanical part is modelled using a simple harmonic equation in 2D. Then:

Figure 11: Refined mesh of the hydraulic domain Figure 12: Multi-1D mesh of the hydraulic domain

Figure 13: Hydraulic channels surrounding the assemblies

$$
\underline{\underline{M}_i} = \text{diag}(m_i)
$$
\n
$$
\underline{\underline{C}_i} = \text{diag}(c_i)
$$
\n
$$
\underline{\underline{K}_i} = \text{diag}(k_i)
$$
\n(11)

$$
\underline{X_i} = {}^t(x_i, y_i, 0) \tag{12}
$$

The fluid forces are assimilated to the pressure forces, neglecting the shear stress effects:

$$
\underline{F}_{Fl \to St}|_{\partial I_i} = -\int_{\partial I_i} P(x,t) \mathbf{u}_{\mathbf{St} \to \mathbf{Fl}} dx
$$
\n(13)

Non-linear effects from the fluid part are then introduced. When the displacement is relatively small, only added mass effect from the fluid part is observable. But in case of large displacement, the effects from the fluid part cannot be reduced to added mass effects.

4.2 Algorithm of the FSI code coupling

The mechanical and hydraulic parts are solved by two different solvers. Here, the mechanical damping is not considered and then $c_i = 0$ for any *i*. Taking into account Eqs. (11) and (12), the fluid-structure problem for each assembly number *i* is discretized as follows:

$$
m_i \ddot{x_i}^{n+1} + k_i x_i^{n+1} = \tilde{f}_i^{n+1}
$$
\n(14)

The Newmark algorithm is applied for the time-marching using the mean-acceleration scheme:

$$
x_{n+1} = x_n + \Delta t \dot{x}_n + \Delta t^2 \left[(1 - 2\beta) \ddot{x}_n + 2\beta \ddot{x}_{n+1} \right]
$$

\n
$$
\begin{aligned}\n\dot{x}_{n+1} &= \dot{x}_n + \Delta t \left[(1 - \gamma) \ddot{x}_n + \gamma \ddot{x}_{n+1} \right] \\
\tilde{f}_{n+1} &= \Phi(f_n)\n\end{aligned}
$$
\n(15)

with $\beta = \frac{1}{4}$ $\frac{1}{4}$, γ = $\frac{1}{2}$ $\frac{1}{2}$. \tilde{f}_{n+1} is an estimation of f_{n+1} at time *n*.

The nature of the transient phenomenon makes this direct code coupling unstable. As a consequence, a damped fixed point algorithm is used in order to ensure the convergence of the coupled problem, with λ empirically determined when the calculation converges for a given time step ∆*t*:

5 SOME RESULTS

In this section, some computational results of the code coupling algorithm using the multi-1D modelling are presented. The assemblies are initially out of their equilibrium position with $a = 3/4$.

5.1 Results of the code coupling within 1 ring

Here, a configuration with one ring of assemblies is considered. It is a first step in order to see the differences on the displacement field of the assemblies with or without cavitation modelling. The frequency is chosen so that the minimum pressure in the domain reaches the value of *Psat* in order to have a simulation case with cavitation and FSI code coupling. In this context, Figures 14 and 15 show respectively the effects of cavitation on the pressure fields and void fraction field.

Figure 14: Pressure field Figure 15: Void fraction field

In comparison with a simulation without cavitation modelling, the pressure can not be lower than the saturation pressure. As a consequence, the restoring forces in the two cases differ from another (see Figure 16). Complete re-condensation of the vapour phase occur short before *t* = 0*.*002*s* and is observable from the change in the variation of the displacement field. After this event, the displacement field cannot be taken into account due to instabilities affecting the pressure field.

Figure 16: Comparison of the displacements without or with cavitation modelling

5.2 Results of the code coupling within 11 rings

Here, 11 rings are considered in order to represent the real case of a SFR core. In this case, the second eigen-frequency of the assemblies is taken $(f = 20 \text{ Hz})$. The pressure fields with or without cavitation modelling are shown in Figures 17 and 18. Vaporization of the fluid occurs next to the center of the core.

Figure 17: Pressure field with 1-phase modelling Figure 18: Pressure field with 2-phase modelling

With the same manner as in the previous case with 1 ring of assemblies, the restoring force on the assemblies with cavitation differs from the one without cavitation modelling as depicted in Figure 19. The end of the displacement curve corresponds to the same numerical instability affecting the pressure field which has been previously mentioned in the case with 1 ring.

Figure 19: Comparison of the assembly displacements without or with cavitation modelling (first ring)

6 CONCLUSIONS

SFR cores are quite sensible to mechanical deformations and such scenarios may lead to cavitation in the liquid region separating the assemblies. In order to assess such cases, an numerical algorithm coupling two-phase flow and structures within a 2D geometrical representation of a core has been presented.

The algorithm coupling cavitating inter-wrapper liquid sodium and structures makes it possible to predict the impact on the displacement field of the assemblies compared to the case without cavitation modelling.

Nevertheless, the presented numerical algorithm has to be enhanced in order to avoid numerical instabilities when the vapour phases completely disappear.

Moreover, a more detailed analysis concerning the numerical dissipation induced by the FSI numerical algorithm (not presented here) has to be led.

As a perspective, the study has to be extended to 3D geometries since the movement of the assemblies also induces a flow recirculation at the top of the core. This flow entering into the inter-wrapper region may then have an additional influence on the FSI.

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